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Studies on the Kinetics of Polymerization of Styrene Initiated by Arsenic Trichloride

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ABSTRACT

The cationic polymerization of styrene initiated by arsenic trichloride $(AsCl_2)$ in the presence of traces of acetic acid (co-

catalyst) at -8, -4, and 0° C for 100 min using the dilatometric technique in an inert atmosphere yielded low molecular weight polymer. The rate of polymerization (R_p) is a direct function

of the concentration of AsCl₃, monomer, and polar solvent, but

inversely proportional to the polymerization temperature and nonpolar solvent. Hydroquinone has no effect on R_n . Various

kinetic parameters have been evaluated and a kinetic scheme is proposed.

INTRODUCTION

A number of cationic initiators, such as Cl_3CCOOH [1], $HClO_4$ [2], and $SnCl_4$ [3], have been used for the polymerization of styrene. How-

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ever, the polymerization of styrene initiated by AsCl_3 has not been reported in detail.

EXPERIMENTAL

Purified styrene (SRL make), solvents, and nonsolvents were used. AsCl₃ (Fuming, Riedal, Germany) was used as received without further purification. Polymerization was carried out in a modified dila-

tometric apparatus [4, 5] (consisting of a 1.5-cm long bulb of 3 mL monomer capacity attached to a 6-cm long capillary of 2.0 mm diameter) at -8, -4, and 0°C (± 0.05°C) for 100 min in an inert atmosphere. A master graph (Fig. 1) was used to convert volume contraction

data into percentage conversion which was used to calculate the rate of polymerization (R_p) using Eq. (3).

If W grams of polymer was obtained from 1 mL of polymerized monomer in time t (in minutes), then

Percentage conversion (c) =
$$\frac{W \times 100}{0.9090}$$
 (1)

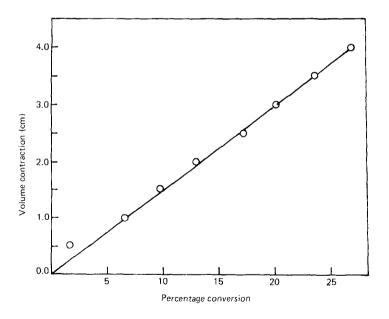


FIG. 1. Master graph showing the relationship between volume contraction and percentage conversion of styrene. Capillary diameter: 2.0 mm.

and

$$R_{p} = \frac{W \times 1000}{104.41 \times 60 \times t}$$
(2)

where 104.41 and 0.9090 are the molecular weight and the density of the styrene, respectively.

Now, using the value of W from Eq. (1) in Eq. (2):

$$R_{p} = \frac{1.4507 \times 10^{-3} \times c}{t}$$
(3)

The intrinsic viscosity (η_{int}) of the polymer, determined in benzene with a Ubbelohde viscometer, was used to calculate the average degree of polymerization (\overline{P}_n) as follows [6]:

$$\overline{P}_{n} = 1.712(\eta_{int})^{1.37}$$
(4)

RESULTS AND DISCUSSION

The polymerization of styrene initiated by $AsCl_3$ (concentration: 0.5-4.0 mol/L) in the presence of traces of acetic acid (cocatalyst) proceeds without an induction period. The results are reported in Table 1. R_p is a direct function of the concentration of $AsCl_3$, and the exponent value of the initiator, determined from the slope of log R_p vs the log concentration of $AsCl_3$ (Fig. 2), is found to be 2.9 \pm 0.10. It is observed that no polymerization occurs in the absence of the cocatalyst. Therefore, it can be assumed that the cocatalyst is responsible for the formation of active centers as shown later by Eqs. (a) and (b) in our kinetic scheme. The propagation step is as usual, but termination is spontaneous as shown by the low molecular weight polymer obtained.

The effect of styrene concentration on R_p and \overline{P}_n was studied by varying the styrene concentration from 2.61×10^{-2} to 5.22×10^{-2} mol/L, as shown in Table 2. R_p and \overline{P}_n are directly influenced by the styrene concentration, and the following quantitative relationship was obtained from the slope of the linear plot between log R_p and the log concentration of styrene (Fig. 3):

$$R_{p} \propto [styrene]^{2 \cdot 0}$$
 (5)

Concentration of AsCl ₃ (mol/L)	$R_p \times 10^4 \text{ mol/L} \cdot \text{s}$		
	-8°C	-4°C	0°C
0.50	2.278	2.035	1.723
1.00	2.637	2.278	1.940
1.50	2.751	2.449	2.129
2.00	2.901	2.581	2.247
2.50	3.084	2.675	2.328
3.00	3.084	2.751	2.449
3.50	3.184	2.675	2.581
4.00	3.202	2.901	2.581

TABLE 1. Effect of AsCl₃ on the Polymerization of Styrene^a

^aStyrene concentration = 2.61×10^{-2} mol/L, time = 100 min.

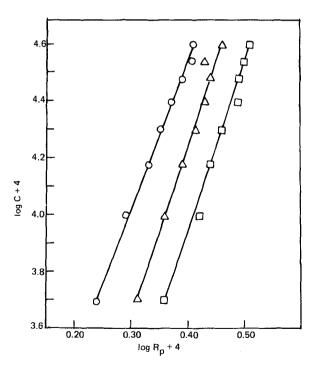


FIG. 2. Log rate of polymerization vs log concentration of $AsCl_3$. Styrene concentration: 2.61×10^{-2} mol/L. Time: 100 min. Temperature: (\circ) 0°C, (\triangle) -4°C, (\Box) -8°C.

TABLE 2. Effect of Styrene Concentration on the Polymerization ofStyrene^a

Concentration of styrene (mol/L) $R_p \times 10^4 \text{ mol/L} \cdot \text{s}$		$\overline{\mathbf{P}}_{\mathbf{n}}$
2.61×10^{-2}	1.723	22.22
3.48×10^{-2}	1.7988	20.00
4.35×10^{-2}	1.988	18.18
5.22×10^{-2}	2.114	17.24

^aAsCl₂ concentration = 0.5 mol/L, time = 100 min, 0°C.

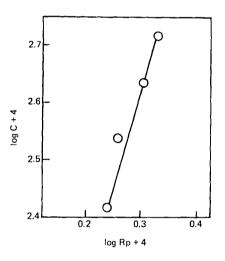


FIG. 3. Log concentration of styrene vs log rate of polymerization. AsCl₃ concentration: 0.5 mol/L. Temperature: 0° C. Time: 100 min.

 R_p is inversely related to the polymerization temperature. An Arrhenius plot (Fig. 4) leads to a value of 1.2 kcal/mol for the activation energy of the overall polymerization reaction. R_p is favored by the polar solvent (CH₃CN) but decreases with a nonpolar solvent (CCl₄) as shown in Table 3. Hydroquinone, however, has no effect on R_p . We could not study the effects of bases as methylamine, pyridine, and aniline on R_p due to the reaction of these bases with AsCl₃.

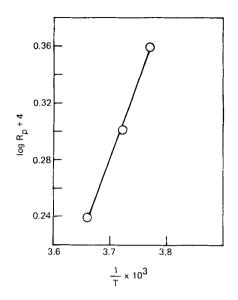


FIG. 4. Log rate of polymerization vs (polymerization temperature)⁻¹. AsCl₃ concentration: 0.5 mol/L. Styrene concentration: 2.61 \times 10⁻² mol/L. Time: 100 min.

TABLE 3. Effect of Additives on R_p of Styrene Initiated by $AsCl_3^a$

Concentration of CH ₃ CN/CCl ₄	$R_p imes 10^4 mol/L$ ·s		
(mol/L)	CH ₃ CN	cc14	
0.0	1.723	1. 723	
1.0	1.789	1.617	
2.0	1.846	1.489	
3.0	1.940	1.362	

^aStyrene concentration = 2.61×10^{-2} mol/L, AsCl₃ concentration = 0.5 mol/L, time = 100 min. 0°C.

POLYMERIZATION OF STYRENE

On the basis of above evidence, it is concluded that $AsCl_3$ acts as a cationic initiator, and the following kinetic scheme is proposed.

The formation of active center (A*) and the initiation step are

$$3I + C \xrightarrow{K_c} A^*$$
 (a)

$$M + A^* \xrightarrow{K_1} M_1^*$$
 (b)

where I, C, and M represent the initiator, the cocatalyst, and the monomer, respectively.

Propagation step:

$$M_n^* + M \xrightarrow{K_p} M_{n+1}^*$$
 (c)

Termination step:

$$M_n^* \xrightarrow{K_t} polymer$$
 (d)

The rates of initiation (R $_{i}$), propagation (R $_{p}$), and termination (R $_{t})$ are given by

$$\mathbf{R}_{i} = \mathbf{K}_{c} \mathbf{K}_{i} [C] [I]^{3} [M]$$
(e)

$$\mathbf{R}_{\mathbf{p}} = \mathbf{K}_{\mathbf{p}}[\mathbf{M}_{\mathbf{n}}^{*}][\mathbf{M}]$$
(f)

$$\mathbf{R}_{t} = \mathbf{K}_{t}[\mathbf{M}_{n}^{*}] \tag{g}$$

Assuming steady-state:

$$[M_{n}^{*}] = \frac{K_{c}K_{i}[C][I]^{*}[M]}{K_{t}}$$
(h)

By keeping the value of M_{n}^{\ast} in Eq. (f), the rate of polymerization is given by

$$R_{p} = \frac{K_{c}K_{i}K_{p}[C][I]^{3}[M]^{2}}{K_{t}}$$
(i)

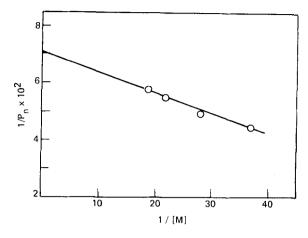


FIG. 5. Reciprocal of average degree of polymerization vs styrene concentration. AsCl₃ concentration: 0.5 mol/L. Temperature: 0°C. Time: 100 min.

and the average degree of polymerization is given by

$$\overline{P}_{n} = \frac{R_{p}}{R_{t}} = \frac{K_{p}[M]}{K_{t}}$$
(j)

A plot of $1/\overline{P}_n$ and 1/[M] (Fig. 5) yields a straight line, the slope of which gives a value [7] of $K_t/K_n = 6.6 \times 10^{-4}$.

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